

## Research Article

# Hydrothermal Synthesis of Nanostructured Manganese Oxide as Cathodic Catalyst in a Microbial Fuel Cell Fed with Leachate

Yuan Haoran,<sup>1,2</sup> Deng Lifang,<sup>1,2</sup> Lu Tao,<sup>1,2</sup> and Chen Yong<sup>3</sup>

<sup>1</sup> Guangzhou Institute of Energy Conversion, Chinese Academy of Sciences, Guangzhou 510640, China

<sup>2</sup> Key Laboratory of Renewable Energy and Gas Hydrate, Chinese Academy of Sciences, Guangzhou 510640, China

<sup>3</sup> Guangzhou Division Academy, Chinese Academy of Sciences, Guangzhou 510070, China

Correspondence should be addressed to Deng Lifang; denglf@ms.giec.ac.cn

Received 14 November 2013; Accepted 27 January 2014; Published 27 February 2014

Academic Editors: B. Cao, Y.-C. Yong, S.-G. Zhou, and L. Zhuang

Copyright © 2014 Yuan Haoran et al. This is an open access article distributed under the Creative Commons Attribution License, which permits unrestricted use, distribution, and reproduction in any medium, provided the original work is properly cited.

Much effort has been devoted to the synthesis of novel nanostructured MnO<sub>2</sub> materials because of their unique properties and potential applications as cathode catalyst in Microbial fuel cell. Hybrid MnO<sub>2</sub> nanostructures were fabricated by a simple hydrothermal method in this study. Their crystal structures, morphology, and electrochemical characters were carried out by FESEM, N<sub>2</sub>-adsorption-desorption, and CV, indicating that the hydrothermally synthesized MnO<sub>2</sub> (HSM) was structured by nanorods of high aspect ratio and multivalve nanoflowers and more positive than the naturally synthesized MnO<sub>2</sub>(NSM), accompanied by a noticeable increase in oxygen reduction peak current. When the HSM was employed as the cathode catalyst in air-cathode MFC which fed with leachate, a maximum power density of 119.07 mW/m<sup>2</sup> was delivered, 64.68% higher than that with the NSM as cathode catalyst. Furthermore, the HSM via a 4-e pathway, but the NSM via a 2-e pathway in alkaline solution, and as 4-e pathway is a more efficient oxygen reduction reaction, the HSM was more positive than NSM. Our study provides useful information on facile preparation of cost-effective cathodic catalyst in air-cathode MFC for wastewater treatment.

## 1. Introduction

Microbial fuel cell (MFC) is a promising biotechnology that utilizes microorganisms as catalysts to decompose organic or inorganic matter and simultaneously harvest electricity, which present a new approach for generating electricity from waste and biomass [1–4]. Air breathing microbial fuel cells, typically characterized by using natural convection air-flow to their cathodes, are attractive for wastewater treatment applications due to their simple single-chamber construction and their unique ability to remove organic matter and generate bioelectricity. In such oxygen cathode system, the function of MFC would be significantly affected by the cathode performance due to the poor kinetics of oxygen reduction reaction (ORR).

To improve ORR and simultaneously maximize the power density, various kinds of electrocatalysts such as Pt [5], lead dioxide [6], iron (III) phthalocyanine(FePc) and cobalt tetramethoxyphenyl porphyrin(COTMPP) [7–10], Prussian blue/polyaniline [11], iron related ethylenediaminetetraacetic

acid [12], Co/Fe/N/CNT [13], and Co-naphthalocyanine [14] have been evaluated for their ORR activity in MFC cathodes and the MFCs all exhibited good performances. However, the high cost of platinum, the toxicity of lead dioxide, long-term instability of the transition metal macrocycles, and phthalocyanines make these alternatives impractical.

In the past decade, manganese dioxide has been studied as one of the most promising cathode catalyst for alkaline fuel cell and metal-air batteries application [15], and several research groups have previously shown that nonprecious manganese dioxide electrocatalysts were highly efficient for catalyzing ORR and lowering overall cost at the same time [16–18]. Recent studies had paid their attention towards carbon nanotubes (CNTs) coated with manganese dioxide and MnO<sub>2</sub> nanoparticles [19–21]. However, very limited efforts have been made to evaluate the activities of nanostructured manganese oxides. Roche et al. [22] found that the power density of the MFC with carbon-supported MnO<sub>2</sub> nanoparticles can reach 161 mW/m<sup>2</sup> compared to 19 mW/m<sup>2</sup> for a benchmark Pt/C at room temperature, and when

using nanostructured  $\text{MnO}_x$  as cathode catalyst the MFC can achieved a peak power density of  $772.8 \text{ mW/m}^3$  [23]. Thus, it is of significant to develop manganese oxides with controllable morphology and nanostructures by using facile methods for enhancing oxygen reduction and lowering the cost of single-chamber MFC for wastewater treatment. In this study, nanostructure manganese oxide prepared by hydrothermal synthesis method is applied on MFC cathode, which shows comparable catalytic capability to naturally synthesized manganese oxide, and it could further facilitate the scaling up of MFC.

## 2. Materials and Methods

**2.1. Catalysts Preparation.** The hydrothermally synthesized nanostructure  $\text{MnO}_2$  (HSM) was synthesized as described elsewhere [24]. Briefly,  $0.2 \text{ g MnSO}_4 \cdot \text{H}_2\text{O}$  and  $0.5 \text{ g KMnO}_4$  were dissolved in  $100 \text{ mL}$  distilled water; then well-mixed aqueous solution of  $\text{KMnO}_4$  and hydrated  $\text{MnSO}_4$  were transferred to a Teflon-lined pressure vessel (QiangQiang Instrument, Shanghai.) and loaded into an oven preheated to  $140^\circ\text{C}$ ; the dwell time for the reaction chose  $8 \text{ h}$  when the nanostructure  $\text{MnO}_2$  was prepared. After the reaction was finished, the pressure vessel cooled to room temperature naturally. The precipitation formed was filtered and washed with distilled water until the pH of the wash water was 7 and finally dried at  $100^\circ\text{C}$  in air. The same amounts of starting materials were left in a beaker overnight for the formation of  $\text{MnO}_2$  precipitate in order to see the structural evolution of nanostructured  $\text{MnO}_2$  from room temperature to the hydrothermal treatment. After the reaction was finished, all operations were the same as the synthesis of nanostructure  $\text{MnO}_2$ .

### 2.2. Characterization of $\text{MnO}_2$

**2.2.1. FESEM.** The morphology of  $\text{MnO}_2$  was characterized with field emission scanning electronic microscopy (FESEM) (HITACHI, S-4800). The specific surface areas of  $\text{MnO}_2$  were measured by the Brunauer-Emmett-Teller (BET) method, in which  $\text{N}_2$  adsorption at  $77 \text{ K}$  was applied and Carlo Erba Sorptometer was used.

**2.2.2. CV.** Cyclic voltammetric (CV) measurements were performed with an Autolab potentiostat (model PGSTAT 30) with a three-electrode system (Ecochemie, Netherlands). The glass carbon electrode (GCE, with a diameter of  $3.0 \text{ mm}$ ) coated by catalyst severs as the working electrode a Pt wire and  $\text{Ag/AgCl}$  (sat. KCl,  $222 \text{ mV}$  versus SHE) were used as the counter and reference electrodes, respectively. CV measurements were performed from  $-0.6 \text{ V}$  to  $0.2 \text{ V}$  at a scan rate of  $100 \text{ mV} \cdot \text{S}^{-1}$  in a  $0.1 \text{ M KOH}$  electrolyte. The electrolyte solution is bubbled with  $\text{O}_2$  or  $\text{N}_2$  to establish aerobic or anaerobic environment, respectively, for  $30 \text{ min}$  prior to each scan series, and  $3 \text{ min}$  between every two scans.

**2.3. MFC Configuration and Operation.** All MFCs were operated at  $30 \pm 1^\circ\text{C}$  in a temperature-controlled incubator (HPG-280H, China). The air-cathode MFC consisted of a plastic (Plexiglas) cuboid chamber ( $2 \times 5 \times 5 \text{ cm}^3$ ) [25] and

with a membrane electrode assembly on one side. Carbon felt ( $8 \times 8 \text{ cm}^2$ , Panex 33160K, Zoltex) was used as the anode. Carbon cloth and cation-exchange membrane was hot-pressed together to be cathode. Titanium wire was inserted inside the carbon felt and carbon cloth to connect the circuit. Active area of the cathode was  $25 \text{ cm}^2$ . For all tests, a  $1000 \Omega$  external resistance was fixed except as noted. And the anode chamber of the MFC was filled with  $40 \text{ mL}$  of leachate (collected during the biodrying pretreatment of MSW from Boluo waste treatment).

**2.4. Data Acquisition.** The cell voltage outputs were measured by a precision multimeter (Victory 9807A, China) and a 16-channel voltage collection instrument (AD8223, China) which continuously monitored the voltages and transferred data to the computer at an interval of  $2 \text{ min}$ . To obtain a polarization curve, the external resistor varied from  $50 \Omega$  to  $10000 \Omega$  when the voltage output approached steady state. The corresponding voltages at different external resistances were recorded and the power output (W), power density ( $\text{W} \cdot \text{m}^{-2}$ ), and current output density ( $\text{A} \cdot \text{m}^{-2}$ ) were calculated according to  $P = U^2/R$ ,  $P = IU/A$ ,  $I = U/RA$ , where  $U(\text{V})$  is the measured voltage,  $I(\text{A})$  is the current,  $R(\Omega)$  is the external resistance, and  $A(\text{cm}^2)$  is the active surface area of the cathode, and individual electrode potentials were measured versus saturated calomel electrode (SCE). The external resistance was fixed at  $1000 \Omega$  throughout all the experiments except as noted.

## 3. Results and Discussion

**3.1. Synthesis and Characterization of the Catalysts.** The nanostructured  $\text{MnO}_2$  is synthesized by hydrothermal method and  $\text{MnO}_2$  (NSM) is precipitated at room temperature naturally. SEM images of the obtained  $\text{MnO}_2$  are displayed in Figure 1. As can be seen from the pictures, the flowerlike whiskers of  $\text{MnO}_2$  were formed as the material prepared at room temperature by natural synthesis, and when hydrothermally treated for  $8 \text{ h}$ , there has been an increase in the size of the individual whiskers which replicates the formation of nanostructured surface with a distinct platelike morphology, and the nanoarchitecture with few rods evolving in addition to nanostructured platelike morphology was observed, the same as Subramanian found [24]. Moreover, the BET surface areas of hydrothermal and NSM were determined to be  $24.91$  and  $111.89 \text{ m}^2/\text{g}$ , respectively (Table 1). For the HSM, the nanostructure increases the BET surface area and is easier for the organic substrates to be adsorbed on the cathodes, and the high BET surface areas of  $\text{MnO}_2$  catalysts could enhance the oxygen absorption and electron acceptance on catalysts surface. Oxygen vacancies created to fulfill an overall charger balance can migrate onto the surface of  $\text{MnO}_2$  nanorod and play important roles in catalysis [18]. With the nanorod surface properties and the existence of oxygen vacancies, the  $\text{MnO}_2$  should substantially increase the oxygen reaction rate and electron acceptance capability. On the other hand, the specific nanorod and platelike structure of the  $\text{MnO}_2$  catalysts facilitated oxygen adhesion.

TABLE 1: Performance of MFCs based on different cathodic catalysts.

Catalyst	OCV (V)	Internal resistance ( $\Omega$ )	Maximum power density ( $\text{mW}/\text{m}^2$ )	Maximum current density ( $\text{A}/\text{m}^2$ )	BET ( $\text{m}^2/\text{g}$ )
Without catalyst	0.33	250	32.11	0.22	—
Naturally synthesized $\text{MnO}_2$	0.47	200	42.05	0.29	24.91
Hydrothermally synthesized $\text{MnO}_2$	0.50	150	119.07	0.49	111.89

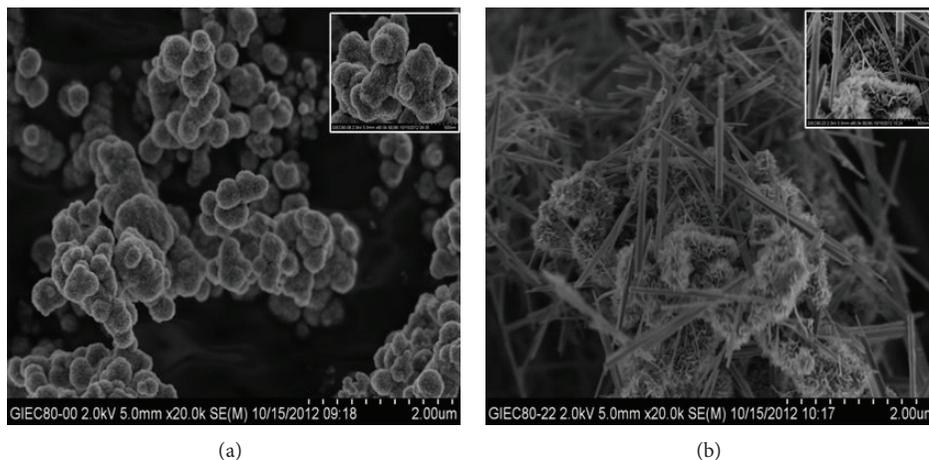


FIGURE 1: SEM images of  $\text{MnO}_2$  prepared by different methods: (a) natural process; (b) hydrothermal process. The inset images are the higher magnifications.

3.2. *Electrochemical Characterization of the Catalysts.* Cyclic voltammograms recorded at scan rate of 100 mV/s for naturally and hydrothermally synthesized  $\text{MnO}_2$  in a 0.1 M KOH electrolyte under aerobic (bubbled with  $\text{O}_2$ ) and anaerobic (bubbled with  $\text{N}_2$ ) environment are shown in Figure 2. It can be seen from the figures that the  $\text{MnO}_2$  possesses a reduction peak ( $-0.5$  to  $-0.3$  V) in aerobic environment but no peak in anaerobic environment (Figure 2), indicating the peak attribution to the catalyzed ORR process.

Comparing with the naturally synthesized  $\text{MnO}_2$ , the peak potential of HSM was  $-0.385$  V versus Ag/AgCl, more positive than that for naturally synthesized  $\text{MnO}_2$  ( $-0.443$  V) and the HSM with a noticeable increase in oxygen reduction peak current (Figure 2). This may suggest an effective disproportionation of the electrogenerated hydrogen peroxide by the HSM nanorods and nanostructured platelike [23]. More importantly, the improved dispersion of nanostructured  $\text{MnO}_2$  favors oxygen adsorption due to its larger BET, facilitating electron transfer through the film and decreasing the ORR over potential. In addition, the presence of oxygenated groups on the surface of cathode catalyst, partially due to oxidation by permanganate, may facilitate oxygen reduction, as reported by Kinoshita [26]. Thus, as the NSM is relatively low adsorption of oxygen and weaker ORR performance, it was expected that between the naturally and hydrothermally synthesized  $\text{MnO}_2$ , the HSM would constitute a more effective cathode catalyst material for MFCs.

3.3. *MFC Performances with Various Catalysts.* The performance of MFCs with the NSM and HSM was evaluated alongside that of the cathode without loading catalyst by

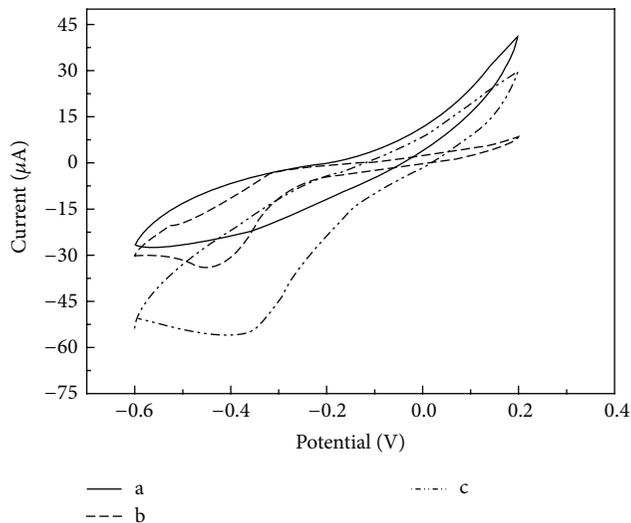


FIGURE 2: Cyclic voltammograms of  $\text{MnO}_2$  for ORR at scan rate of 100 mV/s in 0.1 M KOH. (a) Electrolyte bubbled with  $\text{N}_2$ ; (b) NSM; (c) HSM. (b)-(c) Electrolyte bubbled with  $\text{O}_2$ .

monitoring cell voltage output, anode and cathode polarization, and power density. As shown in Figure 3, a maximum stable voltage of 0.42 V was delivered by the MFC loading with HSM, which was larger than loading with NSM (0.34 V) and without loading catalyst (0.21 V) MFCs achieved. The main reason for the higher power generation of HSM MFC was that HSM possessed high oxygen reduction rates (ORRs), and the low voltage generation of MFC without loading

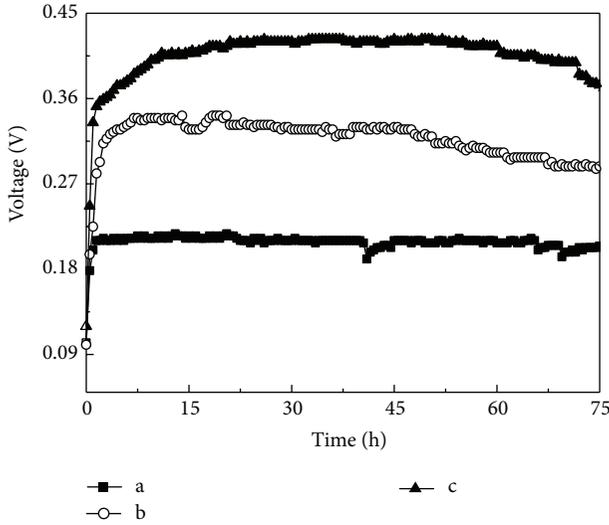


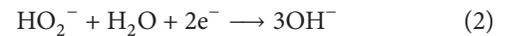
FIGURE 3: The voltage of MFCs with different cathode catalysts. (a) Cathode without loading catalyst; (b) cathode loading with NSM; (c) cathode loading with HSM.

catalyst could be explained by its higher  $R_{in}$  (250  $\Omega$ , as shown in Table 1). The difference of  $R_{in}$  among these MFCs may have been due to the electrical characteristics of the various catalysts, particularly conductivity [18]. Therefore, the sufficient dispersion of nanostructured  $MnO_2$  over the cathode surface resulted in high conductivity and decreased the cathodic resistance, thus achieving a better performance in the MFC loading with HSM.

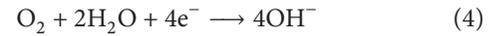
Power densities of different catalysts were compared using a polarization curve measurement. The HSM-based MFC had the highest maximum power density than NSM-based MFC and without loading catalyst MFC. The Maximum power density (based on 25  $cm^2$  projected anode surface area) of 119.07  $mW/m^2$  (about 5.95  $W/m^3$  based on 50  $cm^3$  anode volume, which was about 6.7 times higher than electrochemically deposition nanostructured  $MnO_x$  (772.8  $mW/m^3$ ) [23]), was obtained with HSM as cathode catalyst (with a current density of 0.49  $A/m^2$ ), while a maximum power density of 32.11  $mW/m^2$  and 42.05  $mW/m^2$  was achieved at current densities of 0.22  $A/m^2$  and 0.29  $A/m^2$  without any catalyst or with NSM as cathode catalyst (Figure 4(a)), about 73.03% and 64.68% lower than that with HSM, respectively. The results of this investigation on the dependency of power generation in MFCs are consistent with the results of the BET studies. To understand this observation better, the individual electrode potentials were also measured (Figure 4(b)). The anodic potentials were almost identical in all case due to the matured anodic biofilms, whereas the cathodic potentials were varied, so it was evident that the cathode was the limiting factor in these MFC reactors. For instance, in hydrothermally synthesized  $MnO_2$  MFC, with the increased current densities of 0–0.8  $A/m^2$ , the anode potential increased insignificantly from –0.52 to –0.46 V, whereas the cathode potential dropped from –0.17 to –0.36 V; the larger driving force with an over potential of 0.19 V

required for the cathode compared to the value of 0.06 V required for the anode indicates that power generation from the MFC was dominated by cathode polarization. This is also consistent with the higher OCV (Table 1) and the lower internal resistance of HSM-based MFC than NSM-based MFC, since the lower internal resistance would result in a less ohmic loss and less polarization [27]. Therefore, the results indicated that  $MnO_2$  prepared with a hydrothermal synthesis method could be effectively used as a catalyst in single-chamber air-cathode MFCs to generate current.

**3.4. Oxygen Reduction Mechanisms.** The ORR mechanism in alkaline media on  $MnO_x$  is usually described by the partial 2-electron reduction of  $O_2$  as follows:



Manganese oxides were found to facilitate the decomposition of hydrogen peroxides, according to the  $HO_2^-$  disproportionation reaction (3) [28]. Oxygen can then be reduced according to the reaction (1); the overall reaction is then the apparent 4-electron reduction of  $O_2$ :



The 4-electron process to combine oxygen with electrons and protons directly to produce water as the end product; however, 2-electron processes involving the information of hydrogen peroxide ions as the intermediate. And the hydrogen peroxide ions are corrosive and can degrade the membrane and/or corrode the fuel cell cathode [29, 30]. Furthermore, Cao et al. [31] have studied the mechanism of the ORR in several  $MnO_2$ -catalysed air electrodes. It was found that the ORR is accompanied by the reduction of  $MnO_2$  and that the catalytic activity is dependent on the electrochemical redox activity of these species. In addition, the oxygen reduction at  $MnO_2$ -catalysed air cathode proceeds through chemical oxidation of the surface  $Mn^{3+}$  ions generated by the discharge of  $MnO_2$  rather than through a direct two-electron reduction as previously suggested.

According to Bard and Faulkner [32], the number of electron transfer ( $n$ ) involved in the oxygen reduction at 25°C could be estimated with Randles-sevcik equation (5):

$$i_p = 0.4463(Fn)^{(2/3)}AD_oC_o^*V^{(1/2)}(RT)^{(-1/2)}, \quad (5)$$

where  $i_p$  is peak current (A),  $F$  is Faraday's constant (96485  $C/mol$ ),  $n$  is the number of electrons appearing in half-reaction for the redox couple,  $A$  is the electrode area ( $cm^2$ ),  $D_o$  is the electrolyte's diffusion coefficient ( $cm^2/s$ ),  $C_o^*$  is the concentration of electrolyte at the electrode surface ( $mol/cm^3$ ),  $V$  is the potential scanning rate (v/s),  $R$  is the universal gas constant (8.314  $J/mol \cdot K$ ), and  $T$  is the absolute temperature ( $t+273.15$  K). At 25°C, for  $A$  in  $cm^2$ ,  $D_o$  in  $cm^2/s$ ,  $C_o^*$  in  $mol/cm^3$ , and  $V$  in v/s,  $i_p$  in amperes is as follows:

$$i_p = (2.69 \times 10^5)n^{(2/3)}AD_oC_o^*V^{(1/2)}. \quad (6)$$

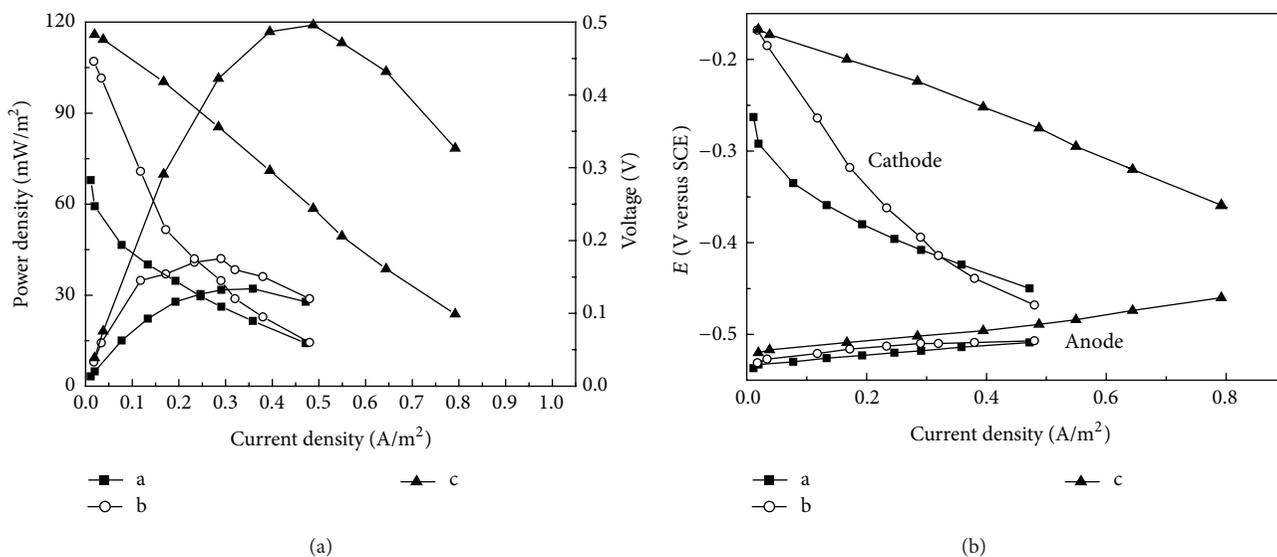


FIGURE 4: Performance of MFC equipped with different catalysts. (a) Cathode without loading catalyst; (b) cathode loading with NSM; (c) cathode loading with HSM.

A in this study was approximately  $0.07 \text{ cm}^2$ . Then according to the data shown in Figure 2,  $n$  in NSM is calculated to be 2.2, but in HSM it is calculated to be 4.3, suggesting that an apparent 2-e reduction of oxygen was achieved on the NSM in alkaline pH solution, but an apparent 4-e reduction of oxygen was achieved on the HSM. This result is the same as the one on  $\text{MnO}_x/\text{C}$  using ring-disc electrode in alkaline solution [22] and the one on electrochemically deposition  $\text{MnO}_x$  nanorods in neutral solution [23]. Moreover, the previous studies indicated that 4-e pathway is more efficient than 2-e pathway [30, 33]. This result further confirmed the previous outcome in this study.

#### 4. Conclusions

In this study, by hydrothermal synthesis method a nanorods evolving in addition to nanostructure platelike morphology  $\text{MnO}_2$  is synthesized, characterized, investigated by SEM and CV methods in alkaline solution and finally incorporated into air-cathode MFCs as cathode ORR catalysts. It is shown that the nanostructure  $\text{MnO}_2$  has quite good capability for ORR catalysis and has an electrochemical activity towards ORR via a 4-e pathway in alkaline solution which is more efficient than 2-e pathway as the NSM undergo. When the  $\text{MnO}_2$  are applied onto air-cathode MFC, the performance of the nanostructured  $\text{MnO}_2$ -based MFC is more efficient and stable than the natural synthesis  $\text{MnO}_2$ . Our findings provide useful information to develop appropriate nanostructured  $\text{MnO}_2$  catalysts towards oxygen reduction in MFC using this facile method. Due to its low cost, easy preparation, and good MFC performance, this catalyst could be a very promising electrocatalyst for air-cathode MFC. It is believed that this efficient and economic catalyst could facilitate the scaling up and commercialization of MFC reactors for practical applications.

#### Conflict of Interests

The authors declare that there is no conflict of interests regarding the publication of this paper.

#### Acknowledgments

This work was financially supported by National 973 project of China (2011CB201501), supported by Projects of International Cooperation and Exchanges NSFC (51161140330), Knowledge Innovation Program of the Chinese Academy of Sciences (NKSCX2-EW-G-1-5), and The Program of Guangdong Province—Chinese Academy of sciences strategic cooperation (2010A090100035).

#### References

- [1] B. Logan, "Generating electricity from wastewater treatment plants," *Water Environment Research*, vol. 77, no. 3, pp. 209–211, 2005.
- [2] B. E. Logan, "Simultaneous wastewater treatment and biological electricity generation," *Water Science and Technology*, vol. 52, no. 1-2, pp. 31–37, 2005.
- [3] K. Rabaey, P. Clauwaert, P. Aelterman, and W. Verstraete, "Tubular microbial fuel cells for efficient electricity generation," *Environmental Science and Technology*, vol. 39, no. 20, pp. 8077–8082, 2005.
- [4] D. R. Lovley, "Bug juice: harvesting electricity with microorganisms," *Nature Reviews Microbiology*, vol. 4, no. 7, pp. 497–508, 2006.
- [5] H. Liu and B. E. Logan, "Electricity generation using an air-cathode single chamber microbial fuel cell in the presence and absence of a proton exchange membrane," *Environmental Science and Technology*, vol. 38, no. 14, pp. 4040–4046, 2004.
- [6] J. M. Morris, S. Jin, J. Wang, C. Zhu, and M. A. Urynowicz, "Lead dioxide as an alternative catalyst to platinum in microbial fuel

- cells," *Electrochemistry Communications*, vol. 9, no. 7, pp. 1730–1734, 2007.
- [7] F. Zhao, F. Harnisch, U. Schröder, F. Scholz, P. Bogdanoff, and I. Herrmann, "Application of pyrolysed iron(II) phthalocyanine and CoTMPP based oxygen reduction catalysts as cathode materials in microbial fuel cells," *Electrochemistry Communications*, vol. 7, no. 12, pp. 1405–1410, 2005.
- [8] S. You, Q. Zhao, J. Zhang, J. Jiang, and S. Zhao, "A microbial fuel cell using permanganate as the cathodic electron acceptor," *Journal of Power Sources*, vol. 162, no. 2, pp. 1409–1415, 2006.
- [9] S. Cheng, H. Liu, and B. E. Logan, "Power densities using different cathode catalysts (Pt and CoTMPP) and polymer binders (Nafion and PTFE) in single chamber microbial fuel cells," *Environmental Science and Technology*, vol. 40, no. 1, pp. 364–369, 2006.
- [10] N. Duteanu, B. Erable, S. M. Senthil Kumar, M. M. Ghangrekar, and K. Scott, "Effect of chemically modified Vulcan XC-72R on the performance of air-breathing cathode in a single-chamber microbial fuel cell," *Bioresource Technology*, vol. 101, no. 14, pp. 5250–5255, 2010.
- [11] L. Fu, S.-J. You, G.-Q. Zhang, F.-L. Yang, X.-H. Fang, and Z. Gong, "PB/PANI-modified electrode used as a novel oxygen reduction cathode in microbial fuel cell," *Biosensors and Bioelectronics*, vol. 26, no. 5, pp. 1975–1979, 2011.
- [12] L. Wang, P. Liang, J. Zhang, and X. Huang, "Activity and stability of pyrolyzed iron ethylenediaminetetraacetic acid as cathode catalyst in microbial fuel cells," *Bioresource Technology*, vol. 102, no. 8, pp. 5093–5097, 2011.
- [13] L. Deng, M. Zhou, C. Liu, L. Liu, C. Liu, and S. Dong, "Development of high performance of Co/Fe/N/CNT nanocatalyst for oxygen reduction in microbial fuel cells," *Talanta*, vol. 81, no. 1-2, pp. 444–448, 2010.
- [14] J. R. Kim, J.-Y. Kim, S. B. Han, K.-W. Park, G. D. Saratale, and S.-E. Oh, "Application of Co-naphthalocyanine (CoNpC) as alternative cathode catalyst and support structure for microbial fuel cells," *Bioresource Technology*, vol. 102, pp. 342–347, 2011.
- [15] Z. Wei, W. Huang, S. Zhang, and J. Tan, "Carbon-based air electrodes carrying MnO<sub>2</sub> in zinc-air batteries," *Journal of Power Sources*, vol. 91, no. 2, pp. 83–85, 2000.
- [16] L. Zhang, C. Liu, L. Zhuang, W. Li, S. Zhou, and J. Zhang, "Manganese dioxide as an alternative cathodic catalyst to platinum in microbial fuel cells," *Biosensors and Bioelectronics*, vol. 24, no. 9, pp. 2825–2829, 2009.
- [17] X. Li, B. Hu, S. Suib, Y. Lei, and B. Li, "Electricity generation in continuous flow microbial fuel cells (MFCs) with manganese dioxide (MnO<sub>2</sub>) cathodes," *Biochemical Engineering Journal*, vol. 54, no. 1, pp. 10–15, 2011.
- [18] X. Li, B. Hu, S. Suib, Y. Lei, and B. Li, "Manganese dioxide as a new cathode catalyst in microbial fuel cells," *Journal of Power Sources*, vol. 195, no. 9, pp. 2586–2591, 2010.
- [19] Y. Zhang, Y. Hu, S. Li, J. Sun, and B. Hou, "Manganese dioxide-coated carbon nanotubes as an improved cathodic catalyst for oxygen reduction in a microbial fuel cell," *Journal of Power Sources*, vol. 196, no. 22, pp. 9284–9289, 2011.
- [20] Y. Chen, Z. Lv, J. Xu et al., "Stainless steel mesh coated with MnO<sub>2</sub>/carbon nanotube and polymethylphenyl siloxane as low-cost and high-performance microbial fuel cell cathode materials," *Journal of Power Sources*, vol. 201, pp. 136–141, 2012.
- [21] M. Lu, L. Guo, S. Kharkwal, H. N. Wu, H. Y. Ng, and S. F. Y. Li, "Manganese-polypyrrole-carbon nanotube, a new oxygen reduction catalyst for air-cathode microbial fuel cells," *Journal of Power Source*, vol. 221, pp. 381–386, 2013.
- [22] I. Roche, K. Katuri, and K. Scott, "A microbial fuel cell using manganese oxide oxygen reduction catalysts," *Journal of Applied Electrochemistry*, vol. 40, no. 1, pp. 13–21, 2010.
- [23] X.-W. Liu, X.-F. Sun, Y.-X. Huang et al., "Nano-structured manganese oxide as a cathodic catalyst for enhanced oxygen reduction in a microbial fuel cell fed with a synthetic wastewater," *Water Research*, vol. 44, no. 18, pp. 5298–5305, 2010.
- [24] V. Subramanian, H. Zhu, R. Vajtai, P. M. Ajayan, and B. Wei, "Hydrothermal synthesis and pseudocapacitance properties of MnO<sub>2</sub> nanostructures," *Journal of Physical Chemistry B*, vol. 109, no. 43, pp. 20207–20214, 2005.
- [25] H. R. Yuan, L. F. Deng, Y. Chen, and S. G. Zhou, "Electricity generation from municipal solid waste leachate using microbial fuel cell technology," *Journal of Basic Science and Engineering*, vol. 20, no. 5, pp. 800–810, 2012.
- [26] K. Kinoshita, *Electrochemical Oxygen Technology*, Wiley-Interscience, New York, NY, USA, 1992.
- [27] L. Zhuang, S. Zhou, Y. Wang, C. Liu, and S. Geng, "Membraneless cloth cathode assembly (CCA) for scalable microbial fuel cells," *Biosensors and Bioelectronics*, vol. 24, no. 12, pp. 3652–3656, 2009.
- [28] L. Mao, D. Zhang, T. Sotomura, K. Nakatsu, N. Koshiba, and T. Ohsaka, "Mechanistic study of the reduction of oxygen in air electrode with manganese oxides as electrocatalysts," *Electrochimica Acta*, vol. 48, no. 8, pp. 1015–1021, 2003.
- [29] M. Chatenet, L. Genies-Bultel, M. Aurousseau, R. Durand, and F. Andolfatto, "Oxygen reduction on silver catalysts in solutions containing various concentrations of sodium hydroxide—comparison with platinum," *Journal of Applied Electrochemistry*, vol. 32, no. 10, pp. 1131–1140, 2002.
- [30] M. Chatenet, M. Aurousseau, R. Durand, and F. Andolfatto, "Silver-platinum bimetallic catalysts for oxygen cathodes in chlor-alkali electrolysis. Comparison with pure platinum," *Journal of the Electrochemical Society*, vol. 150, no. 3, pp. D47–D55, 2003.
- [31] Y. L. Cao, H. X. Yang, X. P. Ai, and L. F. Xiao, "The mechanism of oxygen reduction on MnO<sub>2</sub>-catalyzed air cathode in alkaline solution," *Journal of Electroanalytical Chemistry*, vol. 557, pp. 127–134, 2003.
- [32] A. J. Bard and L. R. Faulkner, *Electrochemical Methods: Fundamentals and Applications*, John Wiley & Sons, New York, NY, USA, 2001.
- [33] K. Gong, F. Du, Z. Xia, M. Durstock, and L. Dai, "Nitrogen-doped carbon nanotube arrays with high electrocatalytic activity for oxygen reduction," *Science*, vol. 323, no. 5915, pp. 760–764, 2009.