

# Synthesis, characterization and application of 1-(2-cyanoethyl)-3-(3-methoxypropane)imidazolium bromide for CO<sub>2</sub> capture

Shantini Ravichandar<sup>1,\*</sup>, Cecilia Devi Wilfred<sup>1</sup>, Chong Fai Kait<sup>1</sup>, and Ng Zhung Gia<sup>1</sup>

<sup>1</sup>Centre of Research in Ionic Liquids (CORIL), Universiti Teknologi Petronas (UTP), Seri Iskandar, 32610, Perak, Malaysia.

**Abstract.** Amine scrubbing is dominating in carbon dioxide (CO<sub>2</sub>) capturing technology because of its high affinity towards CO<sub>2</sub>. However, the drawbacks of amine solvents are its high corrosivity and volatility. Ionic liquids (ILs) have gained a lot of attention in recent years for CO<sub>2</sub> capturing and have been proposed to be one of the promising alternative to the conventional solvents. The objective of this research is to design a new imidazolium based ether-nitrile functionalized ionic liquid of low viscosity to improve CO<sub>2</sub> capturing. The molecular structure of the ionic liquid were confirmed by <sup>1</sup>H NMR, <sup>13</sup>C NMR and FTIR. The thermal properties; glass transition temperature, thermal decomposition temperature, and their physical properties; water content and density were determined. The solubility of CO<sub>2</sub> in the synthesized ionic liquid was measured using pressure drop method. They showed high thermal stability above 200°C and the glass transition temperature was -49.80°C. The CO<sub>2</sub> sorption in the newly synthesized IL was 0.08, 0.12, 0.29, 1.01, 2.30 mol of CO<sub>2</sub>/mol of IL at pressures 1, 5, 10, 15 and 20 bar respectively.

## 1 Introduction

Carbon dioxide has become abundant in the atmosphere due to the extensive burning of fossil fuels. The CO<sub>2</sub> capturing technology is now being the main focus among researchers battling against the dramatic climate change. At present, amine-based solvents are widely used in power plants to capture CO<sub>2</sub> [1]. However, the limitation of amine solvents is that they are highly corrosive and volatile, which is unfriendly to the environment [2]. Besides, they acquire large enthalpy of reaction and amine solvents are also sensitive to degradation in the presence of oxygen [3].

Ionic liquids (ILs) are organic salts which melts below 100°C and are liquid form at room temperature [4]. In light of these factors, ILs have been studied intensively as a potential replacement for amine solvents. This is due to the distinctive characteristics of ILs, i.e. low volatility, high chemical and thermal stability. Furthermore, the added characteristic of ILs is the ability of designing the IL according to the specified task of application.

Imidazolium-based ILs are mostly used in CO<sub>2</sub> solubility due to the presence of acidic hydrogen in its ring structure. CO<sub>2</sub> can act as both Lewis acid and Lewis base. The CO<sub>2</sub> solvation is initiated by some carboxylation reaction at the C2 position of the imidazolium ring [5]. Besides, the ether functionality helps in CO<sub>2</sub> capture whereby the lone pair of electrons present on the oxygen atom takes part in nucleophilic attack with the carbon atom on CO<sub>2</sub> [4]. In a recent

article, ILs with ether functionality has the ability to decrease the viscosity of ILs whereby the alkoxy chain is related to the high rotational flexibility and increases the total free volume [6, 7]. Anions play a vital role in CO<sub>2</sub> dissolution [8]. The common anions of interest are bromide [Br<sup>-</sup>], tetrafluoroborate [BF<sub>4</sub><sup>-</sup>], bis(trifluoromethylsulfonyl)imide [Tf<sub>2</sub>N<sup>-</sup>], hexafluorophosphate [PF<sub>6</sub><sup>-</sup>] and methide. Carbon dioxide solubility is increased as the quantity of fluoroalkyl groups present in anions increased [9].

In the present research, ether-nitrile functionalized imidazolium-based 1-(2-cyanoethyl)-3-(3-methoxypropane)imidazolium bromide, [MOP-imC<sub>2</sub>CN][Br] was synthesized, characterized and tested for the possible application on CO<sub>2</sub> capturing.

## 2 Methodology

### 2.1 Materials

Chemicals such as imidazole and 1-bromo-3-methoxypropane and solvents, i.e. methanol and acetonitrile, were purchased from Merck, Malaysia. Acrylonitrile was of Sigma Aldrich, Malaysia. All chemicals were used without any further purification.

\* Corresponding author: [ravishantini@yahoo.com](mailto:ravishantini@yahoo.com)

## 2.2 Synthesis

### 2.2.1 Synthesis of 1-(2-cyanoethyl)imidazole

The starting material; 1-(2-cyanoethyl)imidazole was synthesized by reacting imidazole with acrylonitrile and methanol as a solvent [10]. The reaction conditions were 50-55°C, under reflux and N<sub>2</sub> atmosphere for 10 h and cooled to room temperature. The impurities were removed by heating at 70°C under vacuum.

### 2.2.2 Synthesis of 1-(2-cyanoethyl)-3-(3-methoxypropane) imidazolium bromide, [MOP-imC<sub>2</sub>CN][Br]

[MOP-imC<sub>2</sub>CN][Br] was prepared by the reaction of 1-(2-cyanoethyl)imidazole with 1-bromo-3-methoxypropane at 70-80°, under reflux and N<sub>2</sub> atmosphere for 48 h. Then, the product was cooled to room temperature resulting [MOP-imC<sub>2</sub>CN][Br].

### 2.2.3 Characterization of ILs

The synthesized IL was characterized using <sup>1</sup>H NMR, <sup>13</sup>C NMR (Bruker Avance 500 MHz) and FTIR (Perkin Elmer Spectrum One). Water content in the ionic liquid was measured using Karl Fischer titrator model Mettler Toledo DL39. Density was measured using density meter (Anton-Paar, DMA 5000 M). The thermal properties and decomposition temperature (T<sub>d</sub>) were measured using thermogravimetric analysis (TGA) and glass transition temperature (T<sub>g</sub>) was measured with differential scanning calorimetry (DSC) (Mettler Toledo model DSC 1).

### 2.2.4 CO<sub>2</sub> sorption study

The possible application of the IL for CO<sub>2</sub> capture was investigated. A custom-made instrument was used for the CO<sub>2</sub> sorption studies (Fig. 1).

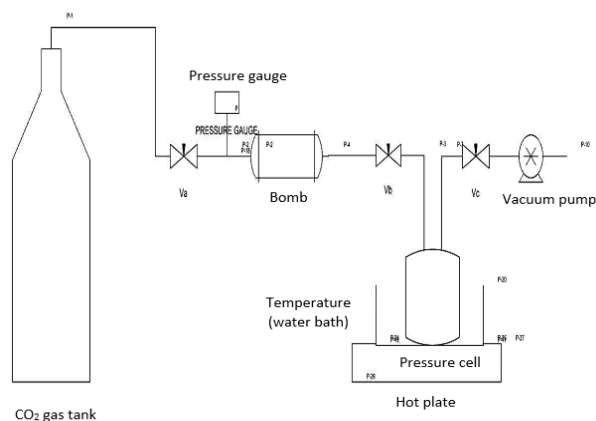


Fig. 1. Schematic diagram for CO<sub>2</sub> gas sorption cell

The measurement technique used was the pressure drop method. Using this method, temperature was held constant and the pressure difference was recorded during gas sorption into the sample. The initial pressure was set at a range of 1 bar to 20 bar. The amount of gas sorbed was calculated from the initial measurement of temperature, volume and pressure and the final measurement of the variables at equilibrium. The calculation was done by converting all three variables into moles of gas using Peng-Robinson equation of state [11].

The mole of CO<sub>2</sub> captured was calculated using equation (1).

$$n = \frac{P_{ini} \cdot V_{tot}}{Z_{ini} \cdot R \cdot T_{ini}} - \frac{P_{eq} (V_{tot} - V_{sample})}{Z_{eq} \cdot R \cdot T_{eq}} \quad (1)$$

where n = mol of CO<sub>2</sub> captured, P<sub>ini</sub> = initial pressure obtained in the absence of sample after expansion of the gas sample from the bomb into the whole system, V<sub>tot</sub> = total volume of system, Z<sub>ini</sub> = compressibility factor (P<sub>ini</sub> × T<sub>ini</sub>), Z<sub>eq</sub> = compressibility factor (P<sub>eq</sub> × T<sub>eq</sub>), P<sub>eq</sub> = pressure at equilibrium, V<sub>sample</sub> = volume of sample, R is the ideal gas constant, T<sub>ini</sub> = initial temperature and T<sub>eq</sub> = temperature at equilibrium. Compressibility factor for CO<sub>2</sub> modifies the ideal gas to account for real gas behaviour [11].

## 3 Results and discussion

### 3.1 NMR analysis

The <sup>1</sup>H-NMR data for the synthesized IL is as shown in Fig. 2 and <sup>13</sup>C-NMR data shown in Fig. 3 respectively. The solvent used during NMR analysis was deuterated acetonitrile.

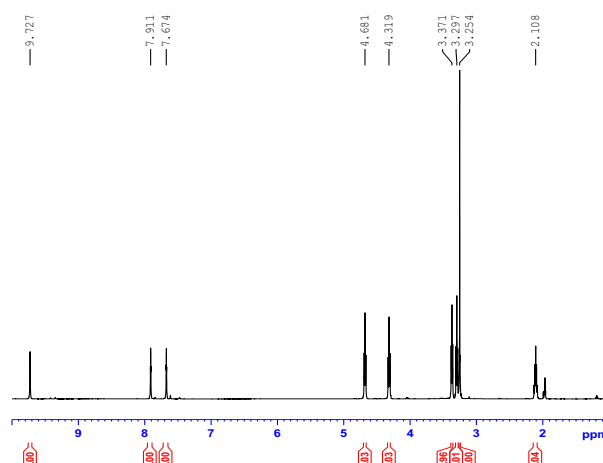
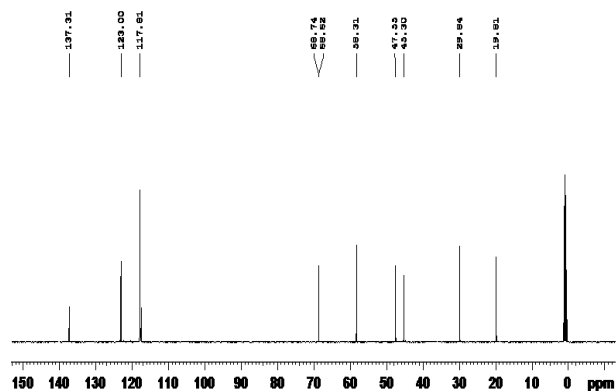
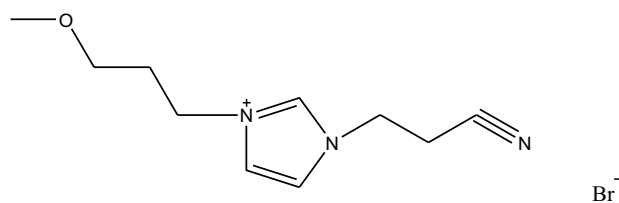


Fig. 2. <sup>1</sup>H-NMR spectra of [MOP-imC<sub>2</sub>CN][Br]



**Fig. 3.**  $^{13}\text{C}$ -NMR spectra of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$



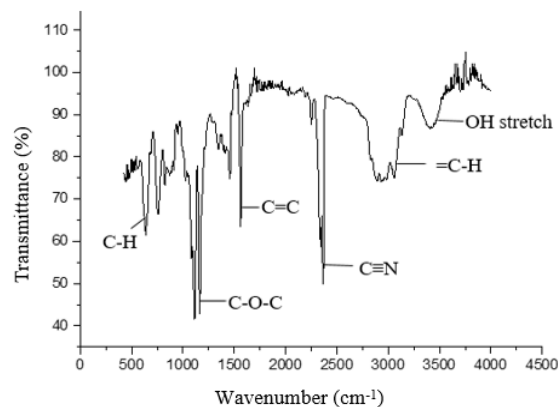
**Fig. 4.** Structure of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$

$^1\text{H}$ -NMR (500MHz,  $\text{CD}_3\text{CN}$ ):  $\delta$  (ppm) 9.73 (s, 1H, NCHN), 7.91 (d, 1H, CHN), 7.67 (d, 1H, CHN), 4.68 (t, 2H,  $\text{CH}_2\text{CH}_2\text{N}$ ), 4.31 (t, 2H,  $\text{CH}_2\text{CH}_2\text{N}$ ), 3.32 (t, 2H,  $\text{CH}_2\text{CH}_2\text{CN}$ ), 3.30 (t, 2H,  $\text{CH}_3\text{OCH}_2$ ), 3.25 (s, 3H,  $\text{CH}_3\text{O}$ ), 2.11 (m, 2H,  $\text{CH}_2\text{CH}_2\text{CH}_2$ );  $^{13}\text{C}$ -NMR (125.77MHz,  $\text{CD}_3\text{CN}$ ):  $\delta$  (ppm) 137.31, 123.00, 117.81, 68.74, 58.31, 47.55, 45.30, 29.84, 19.81.

Spectroscopic data for this ionic liquid were consistent with the literature data [12].

### 3.2 FTIR analysis

The structure of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$  was analysed using Fourier transform infrared (FTIR) and the FTIR spectra obtained is shown in **Fig. 5**. The peaks of wavenumbers 660, 750 and 825  $\text{cm}^{-1}$  are the C-H stretching. A broad peak at about 3400  $\text{cm}^{-1}$  is the O-H stretch which could be due to the presence of water. Peak at wavenumber 2250  $\text{cm}^{-1}$  is due to  $\text{C}\equiv\text{N}$  stretching. Wave numbers 3050-3100  $\text{cm}^{-1}$  and 1400-1600  $\text{cm}^{-1}$  represents  $=\text{C-H}$  stretch and  $\text{C}=\text{C}$  of the aromatic heterocyclic ring respectively. The ether functionality (C-O-C) shows a strong stretching at about wavenumber 1160  $\text{cm}^{-1}$ . Based on the FTIR analysis, it was observed that the IL synthesized is  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$ .



**Fig. 5.** FTIR spectra of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$

### 3.3 Physical properties of $[\text{MOP-imC}_2\text{CN}][\text{Br}]$

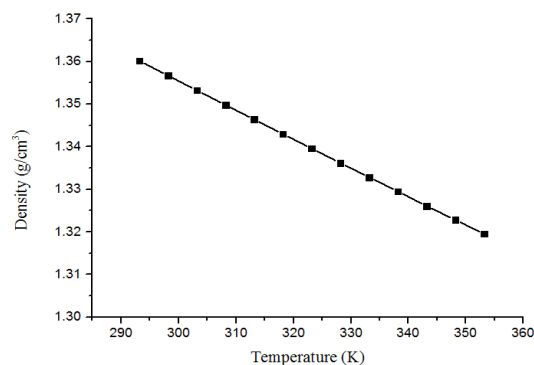
The physical properties of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$  such as the water content, physical appearance and colour at room temperature are shown in **Table 1** below.

**Table 1.** Physical properties of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$

IL	Water content (%)	Colour	Form
$[\text{MOP-imC}_2\text{CN}][\text{Br}]$	0.04	Yellowish	Liquid

#### 3.3.1 Density of $[\text{MOP-imC}_2\text{CN}][\text{Br}]$

The density of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$  at different temperatures is shown in **Fig. 6** below. The plot shows that the density of the synthesized IL decreased linearly with increasing temperature. As shown in Fig. 4, the density of the IL is below 1.36  $\text{g}/\text{cm}^3$  at 293.15 K. Generally, ILs are much denser as compared to water [13].



**Fig. 6.** Density of  $[\text{MOP-imC}_2\text{CN}][\text{Br}]$  as a function of temperature (K)

The density data could be correlated with equation (2).

$$\rho = A + BT \quad (2)$$

where  $\rho$  represents the density of [MOP-imC<sub>2</sub>CN][Br] in g/cm<sup>3</sup>, T is the temperature in Kelvin (K) whereas A and B are the model parameters.

Fitting results are shown in Fig. 4 and the related model parameters are listed in **Table 2** below.

**Table 2.** Fitting result of the experimental density of [MOP-imC<sub>2</sub>CN][Br]

Parameters	[MOP-imC <sub>2</sub> CN][Br]
<i>A</i>	1.5586
<i>B</i> × 10 <sup>4</sup>	-6.774
<i>R</i> <sup>2</sup>	0.9999

### 3.4 Derived thermodynamic property

#### 3.4.1 Thermal expansion coefficient

The thermal expansion coefficient was calculated for the synthesized IL using equation 3 below since the temperature-density relationship was linear.

$$\alpha_P = -\left(\frac{1}{\rho}\right) \cdot \left(\frac{\partial \rho}{\partial T}\right)_P = -(B)/(A+BT) \quad (3)$$

where  $\alpha_P$  represents the thermal expansion coefficient in K<sup>-1</sup>,  $\rho$  is the density, A and B are the fitting parameters of equation (2).

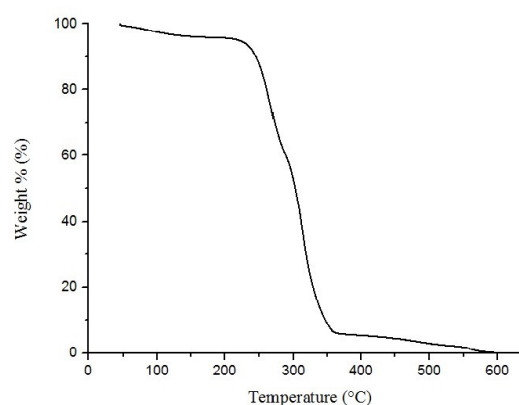
The calculated thermal expansion coefficient is presented in **Table 3**. The thermal expansion coefficient of [MOP-imC<sub>2</sub>CN][Br] obtained in the present work do not change significantly in the temperature range from 293.15 to 353.15 K. Besides, dual functionalized IL has low thermal expansion coefficient [10].

**Table 3.** Density and thermal expansion coefficients,  $\alpha_P$  for [MOP-imC<sub>2</sub>CN][Br]

Temperature (K)	Density (g/cm <sup>3</sup> )	$\alpha_P \times 10^{-4}$ (K <sup>-1</sup> )
293.15	1.360	4.98
298.15	1.357	4.99
303.15	1.353	5.01
308.15	1.350	5.02
313.15	1.346	5.03
318.15	1.343	5.04
323.15	1.340	5.06
328.15	1.336	5.07
333.15	1.333	5.08
338.15	1.330	5.10
343.15	1.326	5.11
348.15	1.323	5.12
353.15	1.320	5.13

### 3.5 Thermal analysis

The IL was heated over a temperature range of 45-600°C at a heating rate of 10°C/min. The synthesized ionic liquid, [MOP-imC<sub>2</sub>CN][Br], has a good thermal stability whereby the onset thermal decomposition started at 246°C with a weight loss of 7.65% and the decompositions ends around 313°C with a weight loss of 97.39%. The T<sub>g</sub> of [MOP-imC<sub>2</sub>CN][Br] was -49.80°C. The TGA profile of [MOP-imC<sub>2</sub>CN][Br] is as illustrated in **Fig. 7**.



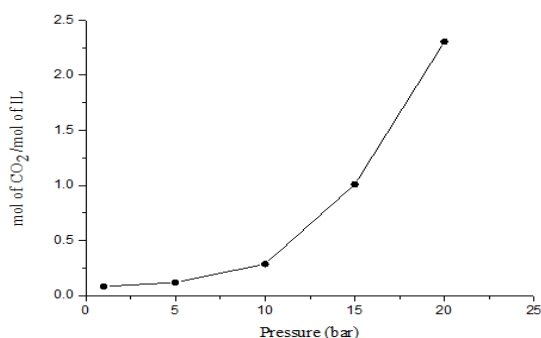
**Fig. 7.** TGA profile of [MOP-imC<sub>2</sub>CN][Br]

A high thermal decomposition temperature of ILs gives a long-term stability of the ILs. Mostly ionic liquids are highly viscous, however, they exhibit a high thermal stability. Therefore, this property enables ILs to be used for a specified application under high temperature which significantly reduces their viscosity [10].

### 3.6 CO<sub>2</sub> solubility

The CO<sub>2</sub> sorption using [MOP-imC<sub>2</sub>CN][Br] was investigated at 25°C using the custom-made gas sorption cell under different pressure condition 1, 5, 10, 15 and 20 bar.

**Fig. 8** shows that CO<sub>2</sub> solubility in [MOP-imC<sub>2</sub>CN][Br] increases with increasing pressure. At equilibrium pressure, P<sub>eq</sub>= 0.73 bar (at 1 bar), the CO<sub>2</sub> absorbed was 0.08 mol of CO<sub>2</sub>/mol of IL whereas at P<sub>eq</sub>=15.82 bar (at 20 bar) the CO<sub>2</sub> shows an absorption of 2.30 mol of CO<sub>2</sub>/mol of IL at 25°C. Ziyada, (2011) has reported that 1-butyl-3-propanenitrile imidazolium dioctylsulfosuccinate [C<sub>2</sub>CN Bim][DOSS] has CO<sub>2</sub> absorption capacity about 2.47 mol of CO<sub>2</sub>/mol of IL at 20 bar [10].



**Fig. 8.** Effect of pressure on CO<sub>2</sub> solubility in [MOP-imC<sub>2</sub>CN][Br] at 25°C

**Table 4** below shows the comparison of experimental solubility data for CO<sub>2</sub> in [C<sub>2</sub>CN Bim][DOSS] and [MOP-imC<sub>2</sub>CN][Br] at 25°C respectively.

**Table 4.** Experimental solubility data for CO<sub>2</sub> in [C<sub>2</sub>CN Bim][DOSS] and [MOP-imC<sub>2</sub>CN][Br] at 25°C

Pressure (bar)	CO <sub>2</sub> solubility (mol of CO <sub>2</sub> /mol of IL)	
	[C <sub>2</sub> CN Bim][DOSS]	[MOP-imC <sub>2</sub> CN][Br]
1	0.06	0.08
5	0.30	0.12
10	0.70	0.29
15	1.28	1.01
20	2.47	2.30

At 5, 10, 15 and 20 bar, [C<sub>2</sub>CN Bim][DOSS] has a higher CO<sub>2</sub> sorption than [MOP-imC<sub>2</sub>CN][Br]. This might be due to the significant role of the DOSS anion present which has a higher affinity towards CO<sub>2</sub> [10]. However, [MOP-imC<sub>2</sub>CN][Br] showed equally good CO<sub>2</sub> sorption whereby the imidazolium ring of the cation is tethered to the ether and nitrile functionality. In addition, at 1 bar, [MOP-imC<sub>2</sub>CN][Br] has slightly higher CO<sub>2</sub> sorption compared to [C<sub>2</sub>CN Bim][DOSS]. The presence of ether functionality enables dipole-quadrupole interactions between the oxygen atoms

present and CO<sub>2</sub> [14]. Besides, high CO<sub>2</sub> solubility can also be correlated with the nitrile group that weakens the cation-anion interaction [7].

Literature shows that CO<sub>2</sub> sorption capacity increases with pressure because at high pressure, physical sorption becomes more significant [15]. From the trend shown in Fig. 8, it is expected that when the pressure is increased to >20 bar, the CO<sub>2</sub> sorption will gradually increase.

## 4 Conclusion

The imidazolium based ether-nitrile functionalized ionic liquid, [MOP-imC<sub>2</sub>CN][Br] has been successfully synthesized, characterized and evaluated for CO<sub>2</sub> sorption. The NMR and FTIR confirmed the structure of the synthesized ionic liquid. The technique used for CO<sub>2</sub> sorption was the pressure-drop method. The results obtained from this study implies that [MOP-imC<sub>2</sub>CN][Br] has a good sorption of CO<sub>2</sub> which is 0.08 mol of CO<sub>2</sub>/mol of IL at P<sub>eq</sub>= 0.73 bar (at 1 bar), and 2.30 mol of CO<sub>2</sub>/mol of IL at P<sub>eq</sub>=15.82 bar (at 20 bar), at 25°C. Besides, the CO<sub>2</sub> sorption can be further enhanced by anion exchange using selective anions which is CO<sub>2</sub>-philic.

The authors acknowledges support from Centre of Research in Ionic Liquids (CORIL) and Fundamental & Applied Sciences Department (FASD), Universiti Teknologi Petronas (UTP). The authors also would like to appreciate and thank E-Science, MOSTI for funding this research.

## References

1. A.B. Rao, E.S. Rubin, Environ. Sci. Technol. **44**, 20 (2002).
2. M. Wang, A. Lawal, P. Stephenson, J. Sidders, C. Ramshaw, Chem. Eng. Res. Des. **89**, 9 (2011).
3. H. Gao, W. Rongwong, C. Peng, Z. Liang, K. Fu, R. Idem, P. Tontiwachwuthikul, Energy Procedia **63**, 1911-1918 (2014).
4. P. Sharma, S.D. Park, K.T. Park, S.K. Jeong, S.C. Nam, I.H. Baek, Bull. Korean Chem. Soc. **33**, 7 (2012).
5. C. Cadena, J.L. Anthony, J.K. Shah, T.I. Morrow, J.F. Brennecke, E.J. Maginn, J. Am. Chem. Soc. **126**, 16 (2004).
6. P. Sharma, S.H. Choi, S.D. Park, I.H. Baek, G.S. Lee, Chem. Eng. J. **181**, 834-841 (2012).
7. Y. Park, K.A. Lin, A.A. Park, C. Petit, Front. Energy Res. **3**, 42 (2015).
8. M. Kankubo, T. Umecky, Y. Hiejima, T. Aizawa, H. Nanjo, Y. Kameda, J. Phys. Chem. B **109**, 29 (2005).
9. M.J. Muldoon, S.N. Aki, J.L. Anderson, J.K. Dixon, J.F. Brennecke, J. Phys. Chem. B, **111**, 30 (2007).
10. A.B. Ziyada, *Thermophysical properties and carbon dioxide solubility of novel room temperature ionic liquids* (2011).

11. E. Torralba-Calleja, J. Skinner, D. Gutierrez-Tauste  
J. Chem. (2013).
12. S. Ravichandar, C.D. Wilfred, F.K. Chong, M.A.  
Abdul Halim, Z.G. Ng, *Contemporary of Sciences:  
Physics, Chemistry and Mathematics*, **2**, (2016).
13. J.S. Wilkes, J. Mol. Catal. A: Chem. **214**, 1 (2015).
14. Y.J. Heintz, L. Sehabiague, B.I. Morsi, K.L. Jones,  
D.R. Luebke, H.W. Pennline, *Energy Fuels* **23**, 10  
(2009).
15. Y. Cheng-Hsiu, H. Chih-Hung, T. Chung-Sung,  
*Aerosol Air Qual Res*, **12** (2011).